

Application No. 09/744,134

Filed: March 21, 2001

TC Art Unit: 1764

Confirmation No.: 3016

AMENDMENT TO THE CLAIMS

1. (Original) Process for the hydrogenation of a sulfur containing feedstock, having a sulfur content of less than 50 ppm, wherein the feedstock is hydrogenated in the presence of a precious metal catalyst, the precious metal being selected from platinum, palladium, rhodium, ruthenium, iridium, osmium and alloys thereof, such as platinum-palladium, and a nickel-catalyst, said process being carried out in such a manner, that the feedstock is contacted initially with the precious metal catalyst followed by contact with a metal oxide and the nickel catalyst, either in combination or sequentially, and wherein the metal oxide has been selected from the oxides of silver, lanthanum, antimony, bismuth, cadmium, lead, tin, vanadium, calcium, strontium, barium, cobalt, copper, tungsten, zinc, molybdenum, manganese and iron.

2. (Canceled)

3. (Currently Amended) Process for the hydrogenation of a sulfur containing feedstock, having a sulfur content of less than 50 ppm, wherein the feedstock is hydrogenated in the presence of a precious metal catalyst, the precious metal being selected from platinum, palladium, rhodium, ruthenium, iridium, osmium and alloys thereof, such as platinum-palladium, and a nickel-catalyst, said process comprising contacting the feedstock first with a mixture of precious metal catalyst and metal oxide, followed by contact with the nickel catalyst, and wherein the metal oxide has been selected ~~from~~ from the oxides of silver, lanthanum, antimony, bismuth, cadmium, lead, tin, vanadium, calcium, strontium, barium, cobalt, copper, tungsten, zinc, molybdenum, manganese and iron.

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4. (Previously Presented) Process according to claim 1, wherein the sulfur content of the feedstock is less than 10 ppm.
5. (Original) Process according to claim 1, wherein the feedstock, after hydrogenation with the precious metal catalyst and before the hydrogenation with the nickel catalyst is contacted with the metal oxide.
6. (Original) Process according to claim 1, wherein the feedstock is simultaneously contacted with the metal oxide and the nickel catalyst.
7. (Previously Presented) Process according to claim 1 or claim 3, wherein the precious metal catalyst is a supported catalyst.
8. (Currently Amended) Process according to ~~claim 1 or claim 3~~ 7, wherein the support of the precious metal catalyst is selected from silica, alumina, silica-alumina, titania, zirconia, zeolites, carbon, clay materials and combinations thereof.
9. (Previously Presented) Process according to claim 1 or claim 3, wherein the precious metal content of the catalyst is between 0.01 and 5.0 wt.%, calculated on the weight of the catalyst.
10. (Previously Presented) Process according to claim 1 or claim 3, wherein the nickel catalyst is Raney nickel or a supported nickel catalyst containing from 0.5 to 99 wt.% nickel.

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11. (Previously Presented) Process according to claim 1 or claim 3, wherein the amount of precious metal catalyst ranges from 1 to 30 vol. % of the total system.

12. (Previously Presented) Process according to claim 1 or claim 3, wherein the weight ratio of nickel catalyst to metal oxide is between 20:1 and 1:20.

13. (Previously Presented) Process according to claim 1 or claim 3, wherein the feedstock is selected from petroleum distillates, resins and solvents.

14. (Canceled)

15. (Previously Presented) Process according to claim 3, wherein the sulfur content of the feedstock is less than 10 ppm.

16. (Previously Presented) Process according to claim 1 or claim 3, wherein:

the precious metal catalyst is a supported catalyst;

the support of the precious metal catalyst is selected from silica, alumina, silica-alumina, titania, zirconia, zeolites, carbon, clay materials and combinations thereof;

the precious metal content of the catalyst is between 0.01 and 5.0 wt.%, calculated on the weight of the catalyst;

the nickel catalyst is Raney nickel or a supported nickel catalyst containing from 0.5 to 99 wt.% nickel;

the amount of precious metal catalyst ranges from 1 to 30 vol.% of the total system;

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the weight ratio of nickel catalyst to metal oxide is between
20:1 and 1:20;

the sulfur content of the feedstock is less than 10 ppm; and

the feedstock is selected from petroleum distillates, resins
and solvents.